

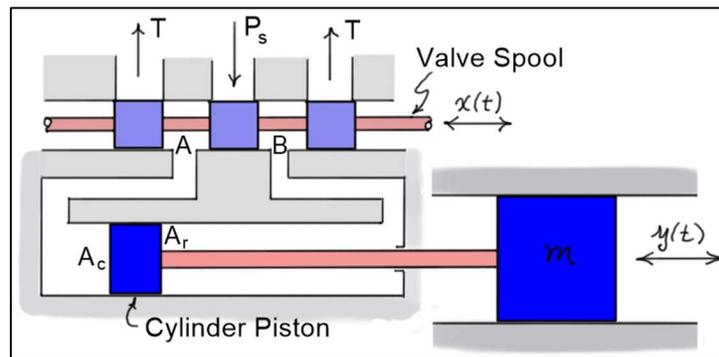
# Introductory Motion and Control

## Hydraulic Positioning System II

References: Dorf and Bishop, *Modern Control Systems*, 9<sup>th</sup> Ed., Prentice-Hall, 2001.  
 Parker *Design Engineer's Handbook: Vol. 1 Hydraulics*, Bulletin 0292-B1-H, 2001.

### Positioning System

- Incompressible fluid
- $A_c$  = cap end piston area
- $A_r$  = rod end piston area
- $m$  = mass of load
- $b$  = damping coefficient
- $P_s$  = constant supply pressure
- $P$  = pressure on the piston
- $p$  =  $\Delta P$ , the change in  $P$
- $X$  = valve spool position
- $x$  =  $\Delta X$ , the change in  $X$
- $Y$  = load position
- $y$  =  $\Delta Y$ , the change in  $Y$



### Operation

- If  $X > 0$ , then the **pressure source** is **applied** to the **A port** of the valve and the **cap end** of the cylinder causing the load to **move** to the **right**. **Return flow** to the tank is through the **B port**.
- If  $X < 0$ , then the **pressure source** is **applied** to the **B port** of the valve and the **rod end** of the cylinder causing the load to **move** to the **left**. **Return flow** to the tank is through the **A port**.

### Flow Model

If  $X > 0$ , then the pressure source is applied to the  $A$  port of the valve. As a result, fluid flows into the cap end of the cylinder and out of the rod end. The flow rate through the valve is a function of  $X$  the spool position and the pressures on either side of the piston.

$$Q_A = g_A(X, P_A) \quad \text{and} \quad Q_B = g_B(X, P_B) \quad (1)$$

To simplify the model, Eqs. (1) can be **linearized** about some **operational** (set) **points**  $(X_0, P_{A0})$  and  $(X_0, P_{B0})$ .

This is done using a **Taylor series expansion**. The change in flow rates can be written as

$$\begin{aligned} q_A &\triangleq \Delta Q_A \approx \left( \frac{\partial g_A}{\partial X} \right)_{X_0, P_{A0}} \Delta X + \left( \frac{\partial g_A}{\partial P_A} \right)_{X_0, P_{A0}} \Delta P_A \\ &= (k_{xA})x - (k_{pA})p_A \end{aligned} \quad (2)$$

$$\begin{aligned}
q_B &\triangleq \Delta Q_B \approx \left( \frac{\partial g_B}{\partial X} \right)_{X_0, P_{B0}} \Delta X + \left( \frac{\partial g_B}{\partial P_B} \right)_{X_0, P_{B0}} \Delta P_B \\
&= (k_{xB})x + (k_{pB})p_B
\end{aligned} \tag{3}$$

The coefficients  $k_{xA}$ ,  $k_{xB}$ ,  $k_{pA}$  and  $k_{pB}$  represent the *derivatives* of the function  $g_A(X, P_A)$  and  $g_B(X, P_B)$  with respect to  $X$  and  $P$ , respectively. The minus sign in the second of Eqs. (2), because the flow rate *decreases* as the pressure in the piston chamber *increases*.

Assuming the fluid is *incompressible*, the piston velocity can be related to the volumetric flow rates as follows.

$$\boxed{Q_A = A_c \dot{Y}} \quad \text{and} \quad \boxed{Q_B = A_r \dot{Y}} \tag{4}$$

Defining variations from the nominal conditions for each port ( $Q = Q_0 + q$ ,  $\dot{Y} = \dot{Y}_0 + \dot{y}$  and  $Q_0 = A\dot{Y}_0$ ), then variations in the piston velocity can be related to changes in the volumetric flow rates as follows.

$$\boxed{q_A = A_c \dot{y}} \quad \text{and} \quad \boxed{q_B = A_r \dot{y}} \tag{5}$$

Combining Eqs. (2), (3) and (5) gives the following equations for the pressure changes at each port.

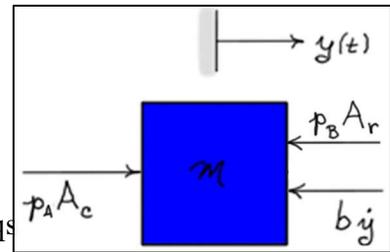
$$\boxed{p_A = (k_{xA}x - A_c \dot{y}) / k_{pA}} \quad \text{and} \quad \boxed{p_B = (-k_{xB}x + A_r \dot{y}) / k_{pB}} \tag{6}$$

### Model for Piston Movement

Assuming  $X > 0$  (flow is entering port  $A$  and leaving port  $B$ ), *Newton's second law* can be used to write the equation of motion of the load.

$$\boxed{\rightarrow \sum F = p_A A_c - p_B A_r - b \dot{y} = m \ddot{y}} \tag{7}$$

*Rearranging* the Eq. (7) and *substituting* for the *pressure changes* from Eqs



$$\boxed{m\ddot{y} + \left( b + \frac{A_c^2}{k_{pA}} + \frac{A_r^2}{k_{pB}} \right) \dot{y} = \left( \frac{A_c k_{xA}}{k_{pA}} + \frac{A_r k_{xB}}{k_{pB}} \right) x} \quad (X > 0) \tag{8}$$

If  $X < 0$ , then  $p_A = (k_{xA}x - A_c \dot{y}) / k_{pA}$ ,  $p_B = (A_r \dot{y} - k_{xB}x) / k_{pB}$ . Substituting these new pressure equations into Newton's law yields the *same form of model* equation as shown in Eq. (8). Note, however, *the coefficients*  $k_{xA}$ ,  $k_{xB}$ ,  $k_{pA}$  and  $k_{pB}$  *will be different* for the two cases, because the nominal pressures (about which the linearization is done) will be different.

## Notes

- If we have a **double rod cylinder**, then  $A_c = A_r$ , so the same model equation holds for motion in both directions. All coefficients will be the same.
- The motion described by Eq. (8) is **second-order, over-damped motion**.
- If the mass of the load is small ( $m \approx 0$ ), then the motion is **first order**.

## Orifice Flow

The volumetric flow rate through a **sharp-edged orifice** can be **approximated** using the equation

$$Q = C_d A \sqrt{2\Delta P / \rho} \quad (9)$$

Here,  $A$  is the orifice area,  $\rho$  is the fluid mass density,  $\Delta P$  is the pressure drop across the orifice, and  $C_d$  is a dimensionless discharge coefficient that depends on Reynolds number and the area reduction. Discharge coefficients in the range  $0.6 \leq C_d \leq 0.8$  are reasonable for a large range of Reynolds numbers and area reductions.

Using Eq. (9) to **model the flow into and out of** the cylinder through the control valve, and assuming the **area of the orifice is proportional to the valve spool displacement**,  $X$ , Eq. (9) can be written as

$$Q_{in} = C_d \ell X \sqrt{2(P_s - P) / \rho}$$
$$Q_{out} = C_d \ell X \sqrt{2(P - P_T) / \rho} \approx C_d \ell X \sqrt{2P / \rho}$$

where  $\ell$  is a characteristic length such that  $A = \ell X$ . Using these two equations, the coefficients in Eqs. (2) and (3) can be estimated as shown below. **For flow into one of the piston chambers**, the coefficients can be estimated to be

$$k_x = \left( \frac{\partial Q_{in}}{\partial X} \right)_{X_0, P_0} = \sqrt{\frac{2}{\rho}} C_d \ell \sqrt{P_s - P_0}$$
$$k_p = \left( \frac{\partial Q_{in}}{\partial P} \right)_{X_0, P_0} = \frac{1}{2} C_d \ell X_0 \sqrt{\frac{2}{\rho}} (P_s - P_0)^{-\frac{1}{2}} = \frac{C_d \ell X_0}{\sqrt{2\rho(P_s - P_0)}}$$

**For flow out of one of the chambers**, the coefficients can be estimated to be

$$k_x = \left( \frac{\partial Q_{out}}{\partial X} \right)_{X_0, P_0} = \sqrt{\frac{2}{\rho}} C_d \ell \sqrt{P_0}$$
$$k_p = \left( \frac{\partial Q_{out}}{\partial P} \right)_{X_0, P_0} = \frac{1}{2} C_d \ell X_0 \sqrt{\frac{2}{\rho}} (P_0)^{-\frac{1}{2}} = \frac{C_d \ell X_0}{\sqrt{2\rho P_0}}$$